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<b>(21) International Application Number:</b> PCT/US91/09150 <b>(22) International Filing Date:</b> 12 December 1991 (12.12.91)  <b>(30) Priority data:</b> 628,000 17 December 1990 (17.12.90) US 649,356 1 February 1991 (01.02.91) US  <b>(71) Applicant:</b> E.I. DU PONT DE NEMOURS AND COMPANY [US/US]; 1007 Market Street, Wilmington, DE 19898 (US).  <b>(72) Inventor:</b> SHIFLETT, Mark, Brandon ; 609 5th Street, Newark, DE 19711 (US).  <b>(74) Agents:</b> SHIPLEY, James, E. et al.; E.I. du Pont de Nemours and Company, Legal/Patent Records Center, 1007 Market Street, Wilmington, DE 19898 (US).		<b>(81) Designated States:</b> AT (European patent), AU, BE (European patent), BR, CA, CH (European patent), DE (European patent), DK (European patent), ES (European patent), FR (European patent), GB (European patent), GR (European patent), IT (European patent), JP, KR, LU (European patent), MC (European patent), NL (European patent), SE (European patent).  <b>Published</b> <i>With international search report.</i>
<b>(54) Title:</b> CONSTANT BOILING COMPOSITIONS OF FLUORINATED HYDROCARBONS  <b>(57) Abstract</b>  Ternary mixtures of pentafluoroethane, difluoromethane and tetrafluoroethane are useful as refrigerants, aerosol propellants, heat transfer media, gaseous dielectrics, fire extinguishing agents, expansion agents for polyolefins and polyurethanes, and as power cycle working fluids.		

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**TITLE****CONSTANT BOILING COMPOSITIONS OF  
FLUORINATED HYDROCARBONS**

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**CROSS-REFERENCE TO RELATED APPLICATION**

This application is a continuation-in-part of U.S. Application  
Serial No. 07/628,000 filed December 17 1990.

**FIELD OF THE INVENTION**

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This invention relates to constant boiling mixtures for use as  
refrigerants, aerosol propellants, heat transfer media, gaseous dielectrics,  
fire extinguishing agents, blowing or expansion agents for polymers such as  
polyolefins and polyurethanes and as power cycle working fluids. More  
particularly, it relates to constant boiling mixtures of fluorinated hydro-  
carbons. Specifically, this invention relates to the use of mixtures of penta-  
20 fluoroethane (HFC-125), difluoromethane (HFC-32) and tetrafluoroethane  
(HFC-134 and/or HFC-134a) as replacements for Refrigerant 502 (R-502),  
a commercial binary azeotrope of chlorodifluoromethane (HCFC-22) and  
chloropentafluoroethane (CFC-115) and the like that have been used as  
25 the refrigerant in numerous commercial applications.

**BACKGROUND OF THE INVENTION**

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Recently the long-term environmental effects of  
chlorofluorocarbons have come under substantial scientific scrutiny. It has  
been postulated that these chlorine-containing materials decompose in the  
stratosphere, under the influence of ultraviolet radiation, to release  
chlorine atoms. Chlorine atoms are theorized to undergo chemical  
reaction with the ozone layer in the stratosphere. This reaction could  
deplete or at least reduce the stratospheric ozone layer, thus permitting  
35 harmful ultra-violet radiation to penetrate the earth's protective ozone  
layer. A substantial reduction of the stratospheric ozone layer could have a  
serious deleterious impact on the quality of life on earth.

Refrigerant 502, the azeotropic mixture of about 47-50

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5 weight percent HCFC-22 and 53-50 weight percent CFC-115 (the  
azeotrope is composed of 48.8 weight percent HCFC-22 and 51.2 weight  
percent CFC-115) has long been used as the refrigerant in most of the  
country's supermarket refrigeration cases. However, since CFC-115 is a  
chloro-fluorocarbon compound which is being phased out by the year 2000,  
10 the industry is required to replace Refrigerant 502 with environmentally  
safer fluorinated hydrocarbons.

The tetrafluoroethanes (HFC-134 and its isomer HFC-134a)  
have been mentioned as possible substitutes. However, the low vapor  
pressures (relatively high boiling points) limit the refrigeration capacity of  
15 these compounds alone, making them undesirable in R-502 applications.  
Also, pentafluoroethane (HFC-125) has been suggested as a replacement  
for R-502, but its energy efficiency (heat removed by the evaporator  
divided by the power to compress the vapor) is 10% lower than R-502.  
Consequently, newly designed equipment would be required to achieve the  
20 refrigeration capacity and energy efficiency currently needed for these  
supermarket applications.

Mixtures of environmentally safe materials might also be  
used if the desired combination of properties could be attained in a simple  
(not constant boiling) mixture. However, simple mixtures create  
25 problems in the design and operations of the equipment used in  
refrigeration systems. These problems result primarily from component  
separation or segregation in the vapor and liquid phases.

Azeotropic or constant boiling mixtures of two or more  
components, where the composition of the vapor and liquid phases are  
30 substantially the same at the temperatures and pressures encountered in  
the refrigeration cycle, would appear to be the answer.

It is an object of the present invention to provide a  
substantially constant boiling composition of at least two hydrofluoro-  
carbons that is low boiling, is non-flammable, and suitable for use as a  
35 refrigerant, aerosol propellant, a heat transfer medium, a gaseous  
dielectric, a fire extinguishing agent, an expansion or blowing agent for  
polymers and as a power cycle working fluid.

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SUMMARY OF THE INVENTION

According to the present invention, a ternary fluorocarbon mixture has been discovered that comprises about 5-90 weight percent pentafluoroethane,  $\text{CF}_3\text{-CHF}_2$ , also known as HFC-125, about 5-90 weight percent difluoromethane,  $\text{CH}_2\text{F}_2$ , also known as HFC-32, and about 5-90 weight percent tetrafluoroethane,  $\text{CF}_3\text{-CH}_2\text{F}$  and  $\text{CHF}_2\text{-CHF}_2$ , also known as HFC-134a and HFC 134, that is suitable for the aforementioned uses, particularly for use in the refrigeration cases found in supermarkets. The substantially constant boiling compositions comprise about 5-59 weight percent HFC-125, 5-59 weight percent HFC-32 and about 5-35 weight percent of at least one of HFC-134 and HFC-134a. The range for HFC-134a is anywhere from about 5-90 weight percent; and, as shown in Table 2, from 15-70 weight percent in mixtures with HFC-125 and HFC-32 were quite satisfactory. As for HFC-134, a range of about 5-45 weight percent, preferably 15-45 weight percent as shown in Table 2, is quite satisfactory.

The compositions of this invention are particularly useful in refrigeration applications since they maintain their stability and their azeotrope-like properties at temperatures of  $-30^\circ\text{F}$  to  $115^\circ\text{F}$  and pressures of 24 psia to 350 psia as shown in the examples hereinafter. As a matter of information, the compositions of this invention may be used successfully at temperatures as low as  $-50^\circ\text{F}$  to temperatures as high as  $300^\circ\text{F}$ .

The novel mixture compositions of the instant invention exhibit differences in dew and bubble points. However, these differences can increase the overall energy efficiency of the refrigeration cycle and be beneficial to refrigeration equipment designers.

There are other ternary and higher blends as shown in Table 2 having desirable characteristics that could be formulated by those skilled in the art from the halocarbons defined and exemplified herein. Another blend that may be formulated for the purposes of this invention is HFC-125/HFC-134a/HFC-134/HFC-32.

The objective of this description is not to identify every possible blend composition, but to illustrate our discovery of the unexpected properties that the ternary (or higher) blends can take on,

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5 depending on the components and the chosen proportions.

For the purpose of this discussion, "near-azeotropic" is intended to mean essentially azeotropic or essentially constant boiling. In other words, included within the meaning of these terms are variable degrees of near-azeotropic behavior depending on the proportions of the components. As is well recognized in this art, there is a range of compositions which contain the same components as the near-azeotrope and demonstrate equivalent properties at other temperatures and pressures, but will behave essentially as those mentioned.

15 The novel ternary mixtures may be used to produce refrigeration by condensing the mixtures and thereafter evaporating the condensate in the vicinity of a body to be cooled.

The novel mixtures may also be used to produce heat by condensing the refrigerant in the vicinity of the body to be heated and thereafter evaporating the refrigerant.

20 The use of non-azeotropic mixtures that exhibit differences in dew and bubble points can be used with countercurrent heat exchangers to offer potential energy efficiency advantages which pure component and azeotropic and near azeotropic mixtures may not exhibit.

25 The novel mixtures have zero ozone depletion potentials (ODP) compared with Refrigerant 502. The ODP are provided in Table 1 for comparison.

30 The novel mixtures have little effect on the global warming potential. The global warming potentials (GWP) of the mixtures/components are listed in Table 1 and R-502 is provided for comparison.

TABLE 1

<u>Refrigerant</u>	<u>Chemical Formula</u>	<u>ODP</u>	<u>GWP</u>
R-502	$\text{CHClF}_2/\text{CClF}_2\text{CF}_3$	.25	5.1
35 HFC-125	$\text{CHF}_2\text{CF}_3$	.0	.65
HFC-134a	$\text{CF}_3\text{CH}_2\text{F}$	.0	.29
HFC-134	$\text{CHF}_2\text{CHF}_2$	.0	.15
HFC-32	$\text{CH}_2\text{F}_2$	.0	.15

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Also, the mixtures can be formulated such that the initial composition or the composition during leakage remains nonflammable. By "nonflammable" is meant a gas mixture in air which will not burn when subjected to a spark igniter according to Flammability Test Method ASTM-E681-85.

10

It should be understood that one or more of the compounds shown in Table 2 can be substituted or combined with the substantially constant boiling ternary mixtures of this invention to provide additional substantially constant boiling mixtures for similar uses while adding advantageous properties unique to the added component(s).

15

TABLE 2

	<u>Nomenclature</u>	<u>Chemical Formula</u>
	HFC-22	$\text{CHClF}_2$
20	HFC-143a	$\text{CH}_3\text{CF}_3$
	HFC-161	$\text{CH}_2\text{FCH}_3$
	FC-218	$\text{CF}_3\text{CF}_2\text{CF}_3$
	Propane	$\text{CH}_3\text{CH}_2\text{CH}_3$
	HFC-23	$\text{CHF}_3$
25	HFC-227ea	$\text{CF}_3\text{CHF}_2\text{CF}_3$

The invention will be more clearly understood by referring to the examples which follow.

30

EXAMPLES 1-12

Evaluation of the refrigeration properties of the novel ternary mixtures of the invention versus Refrigerant 502 are shown in Table 3. The data were generated on a one-ton basis, i.e., based on the removal of heat from a space at the rate of 12,000 BTU/hr.

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**TABLE 3****Comparison of Refrigeration Performance**

10	<u>Conditions</u>							Net Refrig. Effect	<u>Ex</u>
	<u>Evaporator</u>			<u>Condenser</u>					
	<u>Temp</u>			<u>Temp.</u>					
	<u>In</u>	<u>Out</u>	<u>Pres.</u>	<u>In</u>	<u>Out</u>	<u>Pres.</u>			
	<u>(°F)</u>	<u>(°F)</u>	<u>(psia)</u>	<u>(°F)</u>	<u>(°F)</u>	<u>(psia)</u>			
<u>Refrigerants</u>	<u>(°F)</u>	<u>(°F)</u>	<u>(psia)</u>	<u>(°F)</u>	<u>(°F)</u>	<u>(psia)</u>	<u>C.O.P.</u>	<u>(BTU/lb)</u>	<u>Control</u>
R-502	-30	-30	24.0	115	115	281.9	1.89	46.7	Control

<u>Refrigerants</u>	<u>(°F)</u>	<u>(°F)</u>	<u>(psia)</u>	<u>(°F)</u>	<u>(°F)</u>	<u>(psia)</u>	<u>C.O.P.</u>	<u>(BTU/lb)</u>	<u>Ex</u>
R-502	-30	-30	24.0	115	115	281.9	1.89	46.7	Control

Mixtures15 125/134a/32(wt.%)

45/45/10	-34	-25	18.5	119	112	264.3	1.93	68.5	1
75/15/10	-32	-28	24.5	117	113	318.3	1.80	50.0	2
18/57/25	-36	-25	18.6	120	111	270.1	1.97	73.2	3
25/25/50	-34	-27	26.6	117	112	350.3	1.86	81.7	4
50/30/10	-34	-26	21.1	118	112	286.9	1.87	74.2	5
10/70/20	-36	-25	16.9	120	111	244.5	2.01	73.1	6

Mixtures25 125/134/32(wt.%)

45/45/10	-38	-23	16.5	121	109	250.1	1.95	61.7	7
75/15/10	-33	-27	24.0	117	113	315.7	1.80	50.8	8
18/57/25	-39	-21	16.0	123	108	246.7	2.01	77.9	9
25/25/50	-36	-25	24.5	119	111	337.9	1.87	84.2	10
50/30/10	-36	-25	19.7	119	111	281.7	1.87	56.1	11
10/70/20	-39	-21	13.6	123	108	216.8	2.07	78.8	12

35 "Coefficient of Performance" (COP) is the ratio of net refrigeration effect to the compressor work. It is a measure of refrigerant energy efficiency.

"Net Refrigeration Effect" is the change in enthalpy of the refrigerant in the evaporator, i.e., the heat removed by the refrigerant in

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5 the evaporator.

For a refrigeration cycle typified by the above conditions, the COP of the mixtures are either significantly higher or essentially the same as R-502. These mixtures exhibit temperature glides (difference in inlet and exit temperature) through the condenser and evaporator. These glides in temperature vary from 3 to 18°F, depending on the composition of the mixture. In the case of an azeotrope the temperature glide is 0, in the case of a near-azeotropic mixture a temperature glide may be as much as 10°F. However, these temperature glides should not pose any significant problems to equipment manufacturers. In fact, higher temperature glides may be useful to aid designers increase the energy efficiency of their machines. Also, the mixtures have much more capacity than R-502, due to their higher vapor pressures.

Additives such as lubricants, corrosion inhibitors, stabilizers, dyes and other appropriate materials may be added to the novel compositions of the invention for a variety of purposes provided they do not have an adverse influence on the composition for their intended applications.

In addition to refrigeration applications, the novel constant boiling compositions of the invention are also useful as: aerosol propellants, heat transfer media, gaseous dielectrics, fire extinguishing agents, expansion agents for polymers such as polyolefins and polyurethanes, and power cycle working fluids.

### EXAMPLE 13

30 A phase study was made on pentafluoroethane, tetrafluoroethane and difluoromethane to verify the fractionation and change in vapor pressure during a phase change from liquid to vapor.

Blends were prepared in 75 cc stainless steel cylinders consisting of pentafluoroethane, 1,1,1,2-tetrafluoroethane, and difluoromethane. The cylinders were agitated with a magnetic stirrer and submerged in a constant temperature bath at 23.8°C. The vapor pressure was constantly measured using a pressure transducer and the vapor composition was sampled at various times during the experiment and

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- 5 analyzed using a standard gas chromatography method. Initial and final liquid concentrations were also analyzed by gas chromatography. Initial liquid (IQ), final liquid (FQ), vapor composition and vapor pressure data recorded in Tables 4, 5 and 6.

10

TABLE 4

	<u>Sample</u>	<u>Percent Loss</u>	<u>Composition (wt.%)</u>			<u>Vapor Pressure</u>	
			<u>HFC-125</u>	<u>HFC-134a</u>	<u>HFC-32</u>	<u>(psia)</u>	<u>(% Change)</u>
	IQ	0	48.8	17.3	33.9	207.2	0
15	1	6.3	51.0	4.3	44.6	206.0	0.6
	2	12.5	51.8	7.1	41.1	204.8	1.2
	3	18.8	50.9	8.6	40.5	203.6	1.7
	4	25.0	50.9	9.5	39.7	202.2	2.4
	5	31.3	50.6	10.7	38.7	200.5	3.2
20	6	37.5	50.6	11.2	38.1	198.5	4.2
	7	43.8	50.6	12.0	37.5	196.5	5.2
	8	50.4	50.6	12.2	37.2	193.7	6.5
	FQ	50.4	49.4	22.0	28.6	193.7	6.5

25

TABLE 5

	<u>Sample</u>	<u>Percent Loss</u>	<u>Composition (wt.%)</u>			<u>Vapor Pressure</u>	
			<u>HFC-125</u>	<u>HFC-134a</u>	<u>HFC-32</u>	<u>(psia)</u>	<u>(% Change)</u>
	IQ	0	33.9	38.2	27.9	188.4	0
30	1	8.3	41.2	18.8	39.5	184.1	2.3
	2	16.7	40.9	21.9	37.3	180.8	4.0
	3	25.0	40.2	24.0	35.7	178.3	5.4
	4	33.0	38.9	25.3	35.0	174.0	7.6
	5	41.8	37.4	30.3	32.3	171.2	9.1
35	6	51.0	37.3	32.5	30.2	168.7	10.4
	FQ	51.0	30.2	47.0	22.7	168.7	10.4

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TABLE 6

5

	Sample	Percent Loss	Composition (wt.%)			Vapor Pressure	
			HFC-125	HFC-134a	HFC-32	(psia)	(% Change)
	IQ	0	18.7	56.4	24.8	173.2	0
10	1	1.7	26.5	36.9	36.6	172.1	0.4
	2	6.2	25.5	37.5	37.0	169.7	1.4
	3	10.6	25.3	38.5	36.2	164.5	2.4
	4	15.1	24.8	40.2	35.5	162.5	3.5
	5	19.6	24.2	41.6	34.3	160.1	4.5
15	6	24.4	24.4	40.9	34.6	158.4	5.7
	7	28.9	23.8	42.8	31.3	155.6	7.1
	8	33.3	22.8	45.9	31.3	154.0	8.4
	9	37.8	23.1	45.7	31.2	151.3	9.8
	10	42.2	23.4	46.3	31.6	149.0	11.2
20	11	46.7	20.8	49.7	29.5	146.3	12.8
	12	48.9	21.1	51.8	27.1	144.1	13.8
	13	54.4	21.4	51.3	27.3	140.2	15.8
	FQ	54.4	12.7	73.1	14.2	140.2	15.8

25                    These data (Tables 4-6) demonstrate that with more than  
50% of the original charge depleted, the vapor pressure has changed less  
than 16% in all cases. The degree of fractionation depends on the tetra-  
fluoroethane concentration and can be adjusted to give small changes in  
vapor pressure. Mixtures containing 35 wt.% of 1,1,1,2-tetrafluoroethane  
30 (HFC-134a) or less are considered substantially constant boiling since the  
vapor pressure will change less than 10% at 50% leakage. Mixtures  
containing greater than 35 wt.% of 1,1,1,2-tetrafluoroethane are considered  
non-azeotropic as the vapor pressure has changed more than 10% at 50%  
leakage. These mixtures could still be quite useful in many applications,  
35 especially those that require very small sizes. At small charge sizes,  
recharging the mixture due to vapor leakage to return to the desired  
composition does not pose any significant problem. Substituting 1,1,2,2-  
tetrafluoroethane (HFC-134) for HFC-134a would be expected to give

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5 similar results at lower HFC-134 concentrations.

These data also demonstrate that, even though the mixtures fractionate and the vapor pressure decreases, the difluoromethane concentration in both the liquid and vapor phases during leakage also decreases. Therefore, the blend will not become flammable if the initial  
10 concentration is nonflammable. Similar behavior is predicted for the mixture containing HFC-134 instead of HFC-134a.

#### EXAMPLE 14

The ozone depletion potential is based on the ratio of  
15 calculated ozone depletion in the stratosphere resulting from the emission of a compound compared to the ozone depletion potential resulting from the same ratio of emission of CFC-11 which is set at 1.0. A method of calculating ozone depletion potential is described in "The Relative Efficiency of a Number of Halocarbons for Destroying Stratospheric  
20 Ozone", by D. J. Wuebbles, Lawrence Livermore Laboratory Report UCID-18924, January, 1981, and "Chlorocarbon Emission Scenarios: Potential Impact on Stratospheric Ozone", by D. J. Wuebbles, Journal Geophysics Research, 88,1433-1443, 1983.

HFC-125 ( $\text{CF}_3\text{CF}_2\text{H}$ ), HFC-134a ( $\text{CF}_3\text{CFH}_2$ ) or HFC-134  
25 ( $\text{CF}_2\text{HCF}_2\text{H}$ ), and HFC-32 ( $\text{CF}_2\text{H}_2$ ) contain no chlorine atoms; therefore, they have no ozone depletion potential (0 ODP).

The global warming potentials (GWP) of the fluorocarbons were determined using the method described in the "Scientific Assessment of Stratospheric Ozone: 1989", sponsored by the U.N. Environment  
30 Programme. The GWP is a phenomenon that occurs in the stratosphere. It is calculated using a model that incorporates parameters based on the agent's atmospheric lifetime and its infra-red cross-section or its infra-red absorption strength per mole as measured with an infra-red spectrophotometer.

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5 CH-1786-A

CLAIMS:

1. A ternary fluorocarbon mixture comprising about 5-90 weight percent pentafluoroethane, about 5-90 weight percent difluoromethane and 5-90 weight percent of at least one tetrafluoroethane.
2. A ternary fluorocarbon mixture as in Claim 1 which contains 1,2,2,2-tetrafluoroethane and 1,1,2,2-tetrafluoroethane.
3. A mixture as in Claim 1 comprising about 5-59 weight percent pentafluoroethane, about 5-59 weight percent difluoromethane and about 36-65 weight percent of at least one tetrafluoroethane.
4. A substantially constant boiling mixture as in Claim 1 comprising about 5-59 weight percent pentafluoroethane, about 5-59 weight percent difluoromethane and about 5-35 weight percent of at least one tetrafluoroethane.
5. A process for producing refrigeration comprising the steps of condensing the mixture of Claim 1 and, thereafter, evaporating said mixture in the vicinity of a body to be cooled.
6. A process for producing heat comprising the steps of condensing the mixture of Claim 1 in the vicinity of a body to be heated and, thereafter, evaporating said mixture.
7. A process for heating or cooling comprising the step of using the mixture of Claim 1 as a heat transfer media.
8. A process for atomizing a fluid comprising the step of using the mixture of Claim 1 as an aerosol propellant.
9. A process for electrically insulating comprising a step of

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5 using the mixture of Claim 1 as a gaseous dielectric.

10. A process for suppressing a fire comprising a step of using the mixture of Claim 1 as a fire extinguishing agent.

10 11. A process for producing a foamed polymer comprising a step of using the mixture of Claim 1 as a foam expansion agent.

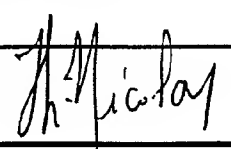
12. A process for delivering power comprising a step of using the mixture of Claim 1 as a power cycle working fluid.

15

## INTERNATIONAL SEARCH REPORT

International Application No.

PCT/US 91/09150

<b>I. CLASSIFICATION OF SUBJECT MATTER</b> (If several classification symbols apply, indicate all) <sup>6</sup>		
According to International Patent Classification (IPC) or to both National Classification and IPC		
Int.Cl. 5 C09K5/04; C09K3/30		
<b>II. FIELDS SEARCHED</b>		
Minimum Documentation Searched <sup>7</sup>		
Classification System	Classification Symbols	
Int.Cl. 5	C09K	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in the Fields Searched <sup>8</sup>		
<b>III. DOCUMENTS CONSIDERED TO BE RELEVANT<sup>9</sup></b>		
Category <sup>10</sup>	Citation of Document, <sup>11</sup> with indication, where appropriate, of the relevant passages <sup>12</sup>	Relevant to Claim No. <sup>13</sup>
P,X	US,A,4 978 467 (SHANKLAND) 18 December 1990 see abstract; claims 1,2,5,8; examples 2,4 ---	1-7,12
X	EP,A,0 400 894 (DU PONT DE NEMOURS) 5 December 1990 see page 3, line 51 - page 4, line 5; claims 1-4 see abstract ---	1-7,12
P,X	EP,A,0 430 169 (MATSUSHITA) 5 June 1991 see claims 1-3; figures 7,8; tables 7,8 ---	1-7,12
P,X	WO,A,9 109 090 (DU PONT DE NEMOURS) 27 June 1991 see page 8, line 10 - page 9, line 9; claims 1,2 ---	1-7,12
<p><sup>10</sup> Special categories of cited documents:</p> <p>"A" document defining the general state of the art which is not considered to be of particular relevance</p> <p>"E" earlier document but published on or after the international filing date</p> <p>"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>"O" document referring to an oral disclosure, use, exhibition or other means</p> <p>"P" document published prior to the international filing date but later than the priority date claimed</p> <p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step</p> <p>"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.</p> <p>"Z" document member of the same patent family</p>		
<b>IV. CERTIFICATION</b>		
Date of the Actual Completion of the International Search	Date of Mailing of this International Search Report	
01 APRIL 1992	15. 04. 92	
International Searching Authority	Signature of Authorized Officer	
EUROPEAN PATENT OFFICE	NICOLAS H.J.F. 	

**ANNEX TO THE INTERNATIONAL SEARCH REPORT  
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